



Sorption and transformation of the reactive tracers Raz and Rru

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# Sorption and transformation of the reactive tracers resazurin and resorufin in natural river sediments

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## Abstract

Resazurin (Raz) and its reaction product resorufin (Rru) have increasingly been used as reactive tracers to quantify metabolic activity and hyporheic exchange in streams. Previous works have indicated that these compounds undergo sorption in stream sediments. We present a series of laboratory column and batch experiments on Raz and Rru transport, sorption, and transformation within sediments with different physico-chemical properties under neutral and alkaline conditions. The data of the column experiments were fitted by a model accounting for physical transport, equilibrium and kinetic sorption, and three first-order reactions. The most likely parameters and their uncertainty were determined by a Markov-Chain Monte Carlo approach. Linear and non-linear sorption isotherms of both compounds were obtained by batch experiments. We found that kinetic sorption dominates sorption of both Raz and Rru, with characteristic timescales of sorption in the order of  $> 80$  min. The linear sorption models for both Raz and Rru appeared adequate for concentrations that are typically applied in field-tracer tests. The supposed two-site sorption model helps interpreting transient tracer tests using the Raz–Rru system.

## 1 Introduction

Resazurin (Raz) undergoes irreversible reduction to resorufin (Rru) in the presence of cellular metabolic activity. Lab experiments (Haggerty et al., 2008; Stanaway et al., 2012) and field-tracer tests (Haggerty et al., 2009; González-Pinzón et al., 2012) have shown that the transformation of Raz to Rru is exceptionally favored in the presence of hyporheic sediments; that is, reaction rates in the presence of colonized sediments are typically three orders of magnitude larger than in the water column, and strongly correlated to respiration (Haggerty et al., 2008; González-Pinzón et al., 2012). This reaction can be used to estimate metabolic activity in hydrologic systems (Haggerty et al., 2009; Argerich et al., 2011). It has also been used to separate effects of in-stream

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mixing processes from exchange processes with comparably immobile, metabolically active zones adjacent to streams in the interpretation of stream-tracer tests (Lemke et al., 2013a; Liao et al., 2013).

In field and column experiments, the breakthrough curves (BTCs) of Raz and Rru usually exhibit tailing and are retarded compared to the BTCs of conservative tracers. Additionally, these experiments have been characterized by an incomplete mass balance between the amount of Raz injected and that of Raz and Rru recovered. The latter observation suggests that Raz and Rru are affected by irreversible sorption and/or transformation to undetected metabolites, preventing complete mass recovery within typical experimental timescales. It is widely known that sorption affects the fate and transport of organic compounds by mass retention on various time scales (Miller and Weber, 1988; Weber et al., 1991; Piwoni and Keeley, 1990), so that sorption processes need to be considered in transient mass transport studies.

To date, little work has been done to characterize the sorption of Raz and Rru. Haggerty et al. (2008) fitted linear and non-linear (Freundlich) isotherms to batch experiments on equilibrium sorption of Rru in stream sediments containing ~ 2 % organic carbon for concentrations of up to 100  $\mu\text{g L}^{-1}$ . The distribution coefficient of the tracers between the solid and aqueous phases in equilibrium, denoted  $K_d$ , derived by the linear sorption isotherm was estimated as 6.63  $\text{L kg}^{-1}$  which corresponds to a retardation factor of up to 60 in sediments. This value most likely overestimates the sorption capacity and is presumably attributed to using a disturbed sample and disregarding the transformation of Rru to non-detected metabolites in the batch sample. Quantifying the sorption of Raz onto natural, metabolically active sediments is difficult by conventional batch experiments due to the rapid reaction of Raz to Rru, so that no such studies have been conducted so far.

In previous studies, sorption of Raz and Rru has been modeled inconsistently. Several studies assumed linear equilibrium sorption (Haggerty et al., 2008; Stanaway et al., 2012; Lemke et al., 2013a), whereas Liao et al. (2013) applied a more sophisticated model considering both equilibrium and kinetic linear sorption. Moreover, some studies

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Rru concentrations of 0, 1, 10, 30, 70, and 100  $\mu\text{gL}^{-1}$ , both at pH 7 and pH 9 (adjusted with 20 mM TAPS and 20 mM MOPS buffer, respectively). All samples were prepared in triplicates. After preparation, all samples were shaken for approximately 40 h at a constant temperature of 20 °C. Subsequently, parts of the supernatant of each sample were filtered (0.45  $\mu\text{m}$  glass fiber filter) and the tracer concentrations were measured by a spectrofluorometer (HORIBA Fluoro-Max-4). The concentration  $s_i$  of the sorbed tracer per mass of solids was calculated by the difference between the initial tracer concentration and the tracer concentration in the aqueous phase after exposure to the sediments over 40 h, normalized by the ratio of solid mass to liquid volume in the samples. The dependence of the sorbed to the dissolved tracer mass was fitted by the standard linear and Freundlich sorption models (Grathwohl, 1998).

### 2.3 Setup of column experiments

All experiments were conducted at a constant temperature of 20 °C to avoid corrections of tracer signals due to temperature fluctuations. All devices and solutions used in the tests were stored in the same room until they reached equilibrium with the room temperature. Except for joints and connections, all tubings were made of stainless steel to avoid sorption of the tracers onto the wall of the tubes.

We used 30 cm long glass columns with an inner radius of 2.5 cm (total volume of 590  $\text{cm}^3$ ). The columns were manually filled with sediment under water to avoid gas entrapment in the pore space. The sediment itself was untreated (i.e. not irradiated) and collected analogously to the sediment for the batch experiments described above. We estimated the effective porosity by fitting the measured fluorescein BTC of each column experiment to the one-dimensional analytical solution of the advection-dispersion equation. In this framework, the porosity is estimated as the specific discharge (“Darcy velocity”), divided by the effective velocity of the tracer. The results indicate that the mean porosity of all columns was 0.45 with only small deviations between the different experiments ( $\sigma = 0.07$ ,  $n = 4$ ). Both connection threads of the column were filled with



possible accuracy of the instruments. The instrumental sampling interval was  $\leq 40$  s which is significantly higher compared to other laboratory studies using Raz and Rru (10–28 min (Stanaway et al., 2012), 15–130 min (Haggerty et al., 2008)). The high temporal resolution of the concentration measurements allowed a detailed analysis of the rising and falling limb of the BTCs, which contain key information regarding sorption processes. Each experiment lasted about 4–5 h (depending on the time until steady-state conditions had been reached).

## 2.4 Mathematical model for reactive transport

The sorption parameters of Raz and Rru were determined by fitting a travel-time based analytical model to the measured BTCs of the tracers in the column experiments. The model considers the formation of Rru as a daughter compound of Raz, decay of Raz and Rru to undetected compounds and mass retention of Raz and Rru due to equilibrium and kinetic sorption processes (Liao et al., 2013).

For the ease of description, we assume in the next paragraphs that the aqueous-phase physical transport of fluorescein, Raz, and Rru within the column may be described by the widely used advection-dispersion equation, amended by reaction and sorption terms for Raz and Rru:

$$\begin{aligned} \frac{\partial c_0}{\partial t} + v \frac{\partial c_0}{\partial x} - D \frac{\partial^2 c_0}{\partial x^2} &= 0 \\ \left(K_1^{\text{eq}} + 1\right) \frac{\partial c_1}{\partial t} + K_1^{\text{kin}} \frac{\partial c_{1,\text{kin}}}{\partial t} + v \frac{\partial c_1}{\partial x} - D \frac{\partial^2 c_1}{\partial x^2} &= (-\lambda_1 - \lambda_{12}) c_1 \\ \left(K_2^{\text{eq}} + 1\right) \frac{\partial c_2}{\partial t} + K_2^{\text{kin}} \frac{\partial c_{2,\text{kin}}}{\partial t} + v \frac{\partial c_2}{\partial x} - D \frac{\partial^2 c_2}{\partial x^2} &= +\lambda_{12} c_1 - \lambda_2 c_2 \\ \frac{\partial c_{i,\text{kin}}}{\partial t} &= k_i (c_i - c_{i,\text{kin}}), \quad i = 1, 2 \end{aligned} \quad (1)$$

subject to the following boundary and initial conditions:

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$$\begin{aligned}
c_0(x=0, t) &= c_{in,0}(t) \\
c_1(x=0, t) &= c_{in,1}(t) \\
c_2(x=0, t) &= 0 \\
c_i(x, t=0) &= 0 \quad i=0,1,2 \\
c_{i,kin}(x, t=0) &= 0 \quad i=1,2
\end{aligned}
\tag{2}$$

in which  $t$  [T] is time, and  $c_i$  [ML<sup>-3</sup>] is the molar aqueous-phase concentration of compound  $i$  with  $i=0$  denoting fluorescein,  $i=1$  Raz, and  $i=2$  Rru.  $v$  [LT<sup>-1</sup>] and  $D$  [L<sup>2</sup>T<sup>-1</sup>] are the effective velocity and the dispersion coefficient, respectively.  $c_{in,0}$  [ML<sup>-3</sup>] and  $c_{in,1}$  [ML<sup>-3</sup>] are the concentrations of fluorescein and Raz in the inflow, respectively, whereas the inflow concentration of Rru is considered zero.  $K_i^{eq} = K_{d,i}^{eq} \rho_b / \theta$  [-] and  $K_i^{kin} = K_{d,i}^{kin} \rho_b / \theta$  [-] are the dimensionless distribution coefficient for the equilibrium sorption and kinetic sorption sites, respectively, whereas  $K_{d,i}^{eq}$  and  $K_{d,i}^{kin}$  [M<sup>-1</sup>L<sup>3</sup>] are the corresponding dimensional distributions coefficients.  $\rho_b$  [ML<sup>-3</sup>] is the bulk density of the dry soil,  $\theta$  [-] denotes effective porosity,  $k$  [T<sup>-1</sup>] is the mass-transfer rate coefficient,  $\lambda_1$  [T<sup>-1</sup>] is the rate coefficient of Raz transformation to undetected products,  $\lambda_{12}$  [T<sup>-1</sup>] is the transformation rate coefficient of Raz to Rru and  $\lambda_2$  [T<sup>-1</sup>] is the rate coefficient of Rru transformation to undetected products.  $c_{i,kin}$  [ML<sup>-3</sup>] is the concentration of the sorbed tracer-compound  $i$  expressed as the corresponding equilibrium aqueous concentration:

$$c_{i,kin} = \frac{s_{i,kin}}{K_{d,i}^{kin}}
\tag{3}$$

in which  $s_{i,kin}$  [MM<sup>-1</sup>] is the mass-related concentration of the kinetically sorbed compound  $i$ .

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We chose to express the effect of the equilibrium sorption by  $K_i^{\text{eq}}$  rather than a retardation factor  $R_i$  or the dimensional distribution coefficient  $K_{d,i}^{\text{eq}}$  to make a direct comparison to  $K_i^{\text{kin}}$  possible. If desired, the values of  $K_i^{\text{eq}}$  can easily be transferred to likewise dimensionless retardation factors by  $R_i = K_i^{\text{eq}} + 1$ .

It is known that the advection-dispersion equation shows deficiencies in exactly reproducing conservative transport, even in homogeneous porous media, whereas transport equations that show similarities to the advection-dispersion equation with a kinetic sorption term lead to better agreements with observed BTCs (Cortis et al., 2004). In this context, fitting the measured BTCs to Eqs. (1–2) may lead to biased results, because the fraction of tailing in the BTCs of Raz and Rru that belongs to non-Fickian conservative transport is misinterpreted as kinetic sorption. We therefore use a formulation of linear reactive transport that relies on the probability density function  $g_0(\tau)$  [ $\text{T}^{-1}$ ] of travel times  $\tau$  [T] rather than the advection-dispersion equation. Transport of all compounds can be expressed by convolution of the concentration in the inflow with a transfer function, because the governing transport processes are linear with respect to tracer concentrations. The transfer functions of Raz and Rru can be derived from the probability density function  $g_0(\tau)$  of travel times and the sorption/transformation parameters listed above.

Because under the given pH conditions, fluorescein is believed to behave conservatively (Smith and Pretorius, 2002; Kasnavia et al., 1999), the travel-time distribution through the column  $g_0(\tau)$  can be obtained by deconvoluting the observed breakthrough curve of fluorescein and the corresponding input signal using a non-parametric approach (Cirpka et al., 2007). A detailed derivation of the travel-time based transport equations can be found in the Appendix A.

A Bayesian approach was adopted in this study to quantify model parameters and their uncertainty. The methods are identical to our previous work (Lemke et al., 2013a; Wöhling et al., 2012) and therefore we subsequently include only a brief summary of the approach.

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Let us consider the transport model  $f$  that simulates the Raz and Rru concentrations summarized as system response  $\mathbf{Y} = \{y_1, \dots, y_n\}$  with length  $n$  using a vector of  $m = 9$  model parameters,  $\mathbf{u} = \{u_1, \dots, u_m\}$ :  $\mathbf{Y} = f(\mathbf{u})$ . Further, we consider that  $\tilde{\mathbf{Y}}$  denotes a vector with the observed concentration data. We then combine the data likelihood,  $p(\mathbf{u}|\tilde{\mathbf{Y}})$  with a prior distribution  $p(\mathbf{u})$  by Bayes theorem to infer the posterior probability density function of the model parameter vector  $\mathbf{u}$ :

$$p(\mathbf{u}|\tilde{\mathbf{Y}}) \propto p(\tilde{\mathbf{Y}}|\mathbf{u})p(\mathbf{u}) \quad (4)$$

We assume measurement errors,  $\sigma_{\text{Raz}} = 2.23 \mu\text{mol m}^{-3}$  and  $\sigma_{\text{Rru}} = 0.12 \mu\text{mol m}^{-3}$  for Raz and Rru concentrations, respectively, which accounts for the higher uncertainty in the measurements of Raz due to its lower quantum yield. We further assume the error residuals to be uncorrelated and normally distributed with constant variance, and replace the data likelihood function  $p(\mathbf{u}|\tilde{\mathbf{Y}})$  by an aggregated likelihood function,  $\ell(\mathbf{u}|\tilde{\mathbf{Y}})$ , for the joint fitting of the Raz and Rru breakthrough curves:

$$\begin{aligned} \ell(\mathbf{u}|\tilde{\mathbf{Y}}) = & -\frac{n_{\text{Raz}}}{2} \ln(2\pi) - \frac{n_{\text{Raz}}}{2} \ln(\sigma_{\text{Raz}}^2) - \frac{1}{2} \sum_{j=1}^{n_{\text{Raz}}} \frac{(y_{\text{Raz},j}(\mathbf{u}) - \tilde{y}_{\text{Raz},j})^2}{\sigma_{\text{Raz}}^2} \\ & - \frac{n_{\text{Rru}}}{2} \ln(2\pi) - \frac{n_{\text{Rru}}}{2} \ln(\sigma_{\text{Rru}}^2) - \frac{1}{2} \sum_{j=1}^{n_{\text{Rru}}} \frac{(y_{\text{Rru},j}(\mathbf{u}) - \tilde{y}_{\text{Rru},j})^2}{\sigma_{\text{Rru}}^2} \end{aligned} \quad (5)$$

where,  $y_{\text{Raz},j}(\mathbf{u})$  and  $y_{\text{Rru},j}(\mathbf{u})$  are the model predicted values for Raz and Rru, respectively, and  $\tilde{y}_{\text{Raz},j}$  ( $j = 1, \dots, n_{\text{Raz}}$ ) and  $\tilde{y}_{\text{Rru},j}$  ( $j = 1, \dots, n_{\text{Rru}}$ ) are the corresponding observations. The parameter vector utilized in Eq. (4) is  $\mathbf{u} = \left\{ K_i^{\text{eq}}, K_i^{\text{kin}}, k_j, \lambda_1, \lambda_{12}, \lambda_2 \right\}$ .

The prior distribution,  $p(\mathbf{u})$  was assumed to be uniform with the following parameter ranges:  $R_1, R_2 = [1 \dots 3]$ ;  $K_1^{\text{kin}}, K_2^{\text{kin}} = [0 \dots 3]$ ;  $k_1, k_2 = [1 \times 10^{-6} \dots 1 \times 10^{-2}]$ ;  $\lambda_1, \lambda_{12}, \lambda_2 = [1 \times 10^{-7} \dots 1 \times 10^{-2}]$ . The choice of these ranges was guided by the preliminary data analysis and previously published values (Haggerty et al., 2008; Liao et al., 2013).

To generate samples from the posterior distribution, we use the differential evolution adaptive metropolis (DREAM<sub>ZS</sub>) adaptive MCMC scheme. The convergence of the DREAM<sub>ZS</sub> runs was monitored by the  $\hat{R}$ -statistic of Gelman and Rubin (1992). In our calculations, we used  $n = 10$  Markov chains and selected the last 10 000 accepted samples after convergence was observed in all chains for the calculation of the posterior parameter tpdfs. All other algorithmic parameters are set to their recommended values. For more details on the parameter inference scheme, please refer to ter Braak and Vrugt (2008), Wöhling and Vrugt (2011), Schoups and Vrugt (2010), and Wöhling et al. (2012).

### 3 Results and discussion

#### 3.1 Batch experiments

A series of batch experiments was conducted in order to obtain equilibrium sorption isotherms for Raz and Rru. Figure 2 shows the mass-related concentrations of the sorbed tracers as function of the aqueous-phase concentration after equilibration. The dashed lines represent linear sorption isotherms, which are in good agreement with the observed data (mean RMSE value of  $5.68 \times 10^{-3} \mu\text{g mL}^{-1}$ ). Applying a Freundlich isotherm did not result in significantly better overall fits (mean RMSE =  $3.03 \times 10^{-3} \mu\text{g mL}^{-1}$ , curves not shown), so that we assume that linear sorption (as described by the single parameter  $K_{d_j}^{\text{batch}} [\text{L}^3 \text{M}^{-1}]$ ) is adequate for the interpretation of field-tracer tests for concentrations of up to  $500 \mu\text{g L}^{-1}$  of Raz and  $100 \mu\text{g L}^{-1}$  Rru. We did not measure the concentrations of Raz and Rru over time in the batch experiments, because any information about kinetic sorption processes would be incomparable to the column tests due to the different solid-to-water ration and the continuous shaking of the batch samples. Thus, the values of  $K_{d_j}^{\text{batch}}$  represent the distribution of the tracers between the liquid phase and the sum of all sorption sites.

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The  $K_{d_i}^{\text{batch}}$  values for Raz and Rru are almost identical at pH 9 (Steinlach:  $0.63 \text{ L kg}^{-1}$  and  $0.66 \text{ L kg}^{-1}$ , respectively and Goldersbach:  $1.00 \text{ L kg}^{-1}$  and  $0.97 \text{ L kg}^{-1}$ , respectively) for the individual sediments. At pH 7, the  $K_{d_i}^{\text{batch}}$ -values are generally higher compared to those at pH 9, and sorption of Raz appears to be stronger than the sorption of Rru. This is consistent with the  $\text{p}K_a$  values of Raz (6.7) and Rru (5.7): At pH 7, about 1/3 of the Raz molecules are in the acidic form, whereas more than 95 % of the Rru molecules remain as anions.

The found values for  $K_{d_i}^{\text{batch}}$  would result in retardation factors of up to 20 within sediments which is much higher compared to retardation factors of Raz and Rru reported in other studies (Lemke et al., 2013b; Liao et al., 2013). Although it is known that batch-reactors have certain disadvantages when used for the determination of sorption isotherms (i.e., conditions in the batch reactors are far from those in the field) and thus may overestimate sorption (Grolimund et al., 1995), the more evident reason for these findings lies in the way how the  $K_{d_i}^{\text{batch}}$ -values were obtained. The calculation of the  $K_{d_i}^{\text{batch}}$ -values is based on the premise that the removal of tracer substances from the aqueous phase in the samples is solely caused by sorption. However, both Raz and Rru may undergo chemical transformation processes, which also results in an effective removal of the tracers. These processes are not accounted for in the standard linear sorption model as applied in the analysis of the batch experiments, because it is impossible to distinguish between decay and sorption as reasons for tracer removal from the aqueous phase. Therefore, the resulting  $K_{d_i}^{\text{batch}}$ -values describe the maximum partition of the tracers between the solids and the liquid (i.e., these values are only valid when no decay of Raz and Rru occurs during the sorption experiment) (Haggerty et al., 2008).

We found that a certain amount of Rru was formed in the batch samples that had a pH of 7 (in average 6 % of the initial molar Raz-concentration), although the combination of the exposure of high temperatures ( $60^\circ\text{C}$  while drying the sediments for several days) and  $\gamma$ -radiation should have destroyed all living cells and also possible

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remains of enzymatic structures. We thus cannot guarantee that the sediments were entirely sterile, so that possibly a small number of living bacteria had enough time to transform a detectable amount of Raz under the advantageous neutral pH conditions in the batch reactors. However, the fact that decay processes occurred in the near-sterile sediments shows that they may not be triggered only by microbial activity.

Unfortunately, we found that the long exposure to the sediments slightly altered the pH in the samples due to the buffer capacity of the carbonate balance. The pH of the pH 7 samples increased to 7.4 and the pH of the pH 9 samples decreased to 8.2 after the exposure to the sediments. However, these alterations are fairly small and the difference in pH between the samples is still big enough, so that the conclusions drawn from the batch experiments with respect to the pH remain unaffected.

### 3.2 Colum experiments

Figure 3 shows the observed BTCs and the model fits obtained by the most likely parameters for all tracers in the 4 column experiments. The measured data are plotted as markers, but the temporal resolution was so high that they appear as continuous lines. All subplots of Fig. 3 also contain inlays showing the same BTCs in a semilog-scale to highlight the tails of the BTCs. Note that only fluorescein and Raz were injected, whereas the measured Rru originates solely from the Raz-to-Rru reaction. The modeled curves fit the measured data very well in all cases (RMSE between  $1.54 \times 10^{-4}$  and  $6.67 \times 10^{-3} \mu\text{molL}^{-1}$ ). One exception is the fit for Raz for the Steinlach sediment at pH 7 (RMSE  $1.18 \times 10^{-2} \mu\text{molL}^{-1}$ ) where we observed small discrepancies between modeled and measured data in parts of the rising and falling limbs. We attribute these differences to technical problems of the fluorometer, and thus neglected the respective parts in the fitting of the BTCs.

Table 2 lists the most likely values of all parameters introduced in Eqs. (6–8) and their associated uncertainties. The uncertainty of each parameter is quantified by the standard deviation of the posterior parameter distribution. All absolute uncertainties are generally very small. The relative errors are smaller than 10 % for the parameters  $R_i$ ,

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$K_i$ ,  $k_i$  and  $\lambda_{12}$  (with the exception of  $k_{Raz}$  which has a relative error of 17%), whereas the decay coefficients  $\lambda_1$  and  $\lambda_2$  have relative errors of around 200% in some cases. However, the estimated parameter values for these decay coefficients are extremely low ( $0.04\text{--}3.68 \times 10^{-5} \text{s}^{-1}$ ) so that the model is not sensitive to small changes in these parameter values.

As listed in Table 2, the values for  $K_i^{\text{eq}}$  at pH 9 are very close to 0 in both sediments (which is equivalent to retardation factors close to 1, see Sect. 2.4), suggesting that equilibrium sorption is negligible under alkaline conditions. Again, these findings agree well with the  $pK_a$  values of Raz and Rru being 6.7 (Erban and Hubert, 2010) and 5.7 (Kangasniemi, 2004), respectively, implying that these compounds occur almost entirely in their anionic form at pH 9 (see Sect. 3.1). At this pH, the mineral surfaces of the sediments used here are most likely predominantly negatively charged as well (Hingston et al., 1972). Consequently, the electrostatic repulsion of mineral surfaces and dissolved tracers hinder sorption. At pH 7, by contrast, equilibrium sorption may be important, even though not consistently among the tracers and sediments: Raz exhibits equilibrium sorption at Steinlach sediments,  $R_{Raz} = 1.2$ , and Rru at Goldersbach sediments,  $R_{Rru} = 1.3$ .

Kinetic sorption is more important than equilibrium sorption for both compounds in both sediments at both pH values, as can be seen from the distribution coefficients  $K_i^{\text{kin}}$  between kinetic sorption sites and water listed in Table 2. For the Steinlach sediment,  $K_i^{\text{kin}}$ -values for both Raz and Rru and both pH conditions are fairly uniform with values between 0.29 and 0.82, whereas  $K_i^{\text{kin}}$ -values for the Goldersbach sediment show a higher degree of variability. In particular,  $K_{Rru}^{\text{kin}}$  of the Goldersbach sediment exhibits the highest values (1.35–1.64) at both pH 7 and pH 9. The comparison of the two sediments types reveals that in average the values for  $K_i^{\text{kin}}$  are slightly higher for Goldersbach sediment compared to the Steinlach sediment. Since the Goldersbach sediment also has a higher porosity and surface area (which includes intraparticle pores) compared to the Steinlach sediment (see Table 1), it is likely that diffusive transport into

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or out of intraparticle pores of the sediment grains is a dominant process leading to kinetic sorption under the given pH conditions.

In order to compare the findings from the column experiments to the values of  $K_d^{\text{batch}}$ , we computed the equivalent distribution coefficient in the column experiments  $K_d^{\text{column}}$  by:

$$K_{d_i}^{\text{column}} = \frac{(K_i^{\text{eq}} + K_i^{\text{kin}}) \theta}{\rho_b} \quad (6)$$

in which  $\theta$  [-] is the effective porosity in the column derived from the fluorescein data (see Sect. 2.2) and  $\rho_b$  [ML<sup>-3</sup>] is the bulk dry density of the sediment (see Table 1). The respective results are listed at the bottom of Table 2.

The  $K_{d_i}^{\text{batch}}$ -values significantly exceed the  $K_{d_i}^{\text{column}}$ -values in all cases (Table 2), so that the sorption of the tracers appears to be generally stronger in the batch-reactors than in the columns. However, the findings from the batch experiments systematically overestimate the sorption capacity of Raz and Rru (see Sect. 3.1), and it is likely that the column experiment setup better represents field conditions in stream sediments, thus providing more realistic information about sorption characteristics of the compounds.

In other studies, retardation factors between 2 and 2.5 have been found (Haggerty et al., 2009; Stanaway et al., 2012). However, these studies did not consider kinetic sorption. If we add the sorption strength of kinetic and equilibrium sites  $R_i^{\text{tot}} = K_i^{\text{eq}} + K_i^{\text{kin}} + 1$ , which is valid for transport time scales much larger than  $k_i^{-1}$ , we obtain similar numbers.

The values for the rate coefficient  $k_i$  of kinetic sorption vary between  $1.97 \times 10^{-4} \text{ s}^{-1}$  and as much as  $50.67 \times 10^{-4} \text{ s}^{-1}$  and no evident correlations of  $k_i$  with the sediment type or pH are identifiable. The inverse of  $k_i$  is a characteristic time of sorption. In our experiments, the values for  $k_i^{-1}$  lie between 3 and 85 min. In comparison, the mean residence times of the tracers in the columns were about 15 min. This implies that the

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quickest kinetic sorption process (Rru in Steinlach sediments,  $k_{\text{Rru}}^{-1} \approx 3$  min) was not distinguishable from equilibrium sorption, the second quickest kinetic sorption process (Raz in Goldersbach sediments,  $k_{\text{Raz}}^{-1} \approx 8$  min) almost reach equilibrium during the passage through the column, whereas the sorption kinetics in the other cases (Raz in Steinlach sediments and in Goldersbach sediments) could not be neglected.

The rate coefficients for decay of Raz ( $\lambda_1$ ) and Rru ( $\lambda_2$ ) to non-detected compounds are generally very small in all experiments (between  $0.44 \times 10^{-5} \text{ s}^{-1}$  and  $3.68 \times 10^{-5} \text{ s}^{-1}$ ) so that even in case of the highest rate only about 3% of the tracers had been converted to non-detected products after contact times with the sediments of 15 min (approximate mean travel time of the tracers through the columns). Argerich et al. (2011) reported a positive relation between organic matter content of the sediment and decay coefficients. In contrast, we could not find any clear relationship between the decay rate coefficients and the type of sediment used or the pH applied in our experiments.

The reaction rate of Raz to Rru ( $\lambda_{12}$ ) strongly depends on pH which can clearly be seen by the different plateau concentrations of Rru in Fig. 2. At pH 7,  $\lambda_{12}$  reaches values of  $4.15 \times 10^{-4} \text{ s}^{-1}$ – $5.72 \times 10^{-4} \text{ s}^{-1}$  which is about one order of magnitude higher compared to values of the same parameter at pH 9 ( $4.45 \times 10^{-5} \text{ s}^{-1}$ – $6.67 \times 10^{-5} \text{ s}^{-1}$ ). Thus, at high pH, the reaction of Raz to Rru may be as important as the decay of the tracers to non-detectable compounds (Goldersbach sediment:  $\lambda_1 = 3.68 \times 10^{-5} \text{ s}^{-1}$  and  $\lambda_{12} = 4.45 \times 10^{-5} \text{ s}^{-1}$ ). While it is known that aerobic respiration depends on pH conditions (Baker et al., 1982; Wang et al., 2006; McKinley and Vestal, 1982), the sporadic measurements of dissolved oxygen taken during the column experiments were inconclusive with respect to pH effects on the respiration rates. An alternative interpretation would be that the proportionality factor relating Raz-to-Rru transformation rates to respiration rates depends on pH, which is possible because the standard biochemical pathway of Raz by reduction of NADH/H<sup>+</sup> or NADPH/H<sup>+</sup> involves an acid-base reaction.

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## 4 Implications for stream-tracer tests

We have found that Raz and Rru do not behave conservatively in sediments, so that sorption of Raz and Rru may not be negligible when interpreting tracer-test data. If not considered, the effects of sorption might misleadingly be captured by parameters that address other processes in standard modeling approaches, resulting in an erroneous characterization of hyporheic exchange and microbial activity in the hyporheic zone. The column experiments showed that under alkaline conditions (pH 9) equilibrium sorption plays a minor role while kinetic sorption might still be important. In general, kinetic sorption seems to dominate sorption in local equilibrium in all our test cases on the time scale of these experiments ( $\approx 15$  min).

We have shown that, in spite of their similar molecular structure, Raz and Rru show different sorption behavior in most of our test cases, so that assuming identical sorption characteristics (as it has been done in previous studies) might be an oversimplification.

We have further shown that linear sorption of Raz and Rru is feasible for concentrations that typically occur during field tracer tests. However, we could not identify clear relations of the physicochemical properties of the parameters (especially the organic carbon content) with sorption characteristics, which makes predicting sorption of Raz and Rru in unknown sediments difficult.

We have furthermore demonstrated that the reaction rate coefficient of Raz to Rru,  $\lambda_{12}$ , differs between the two pH-conditions used in this study. Respiration is likely to be different for different pH as well, so that the change in the reaction rate may result from a change in respiration rate, but it is beyond the scope of this study to determine the mechanisms behind the relation between pH and  $\lambda_{12}$ . Although the decay mechanisms of Raz and Rru to undetected products still ultimately remain unclear, we have found strong evidence that these reactions are not primarily driven by microbial activity.

For stream-tracer tests we suggest (1) acknowledging that Raz and Rru have different sorption properties, (2) accounting for both kinetic and equilibrium sorption (especially when the river sediments are known to have a distinct inner porosity) and

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(3) checking the validity of linear sorption for studies where tracer concentrations exceed the concentrations that were used in this study. In previous studies (Lemke et al., 2013b, Liao et al., 2013), we have determined the sorption and reaction parameters together with parameters describing in-stream transport and hyporheic exchange by fitting stream-tracer data to complex models. This approach leads to apparent parameters, presumably valid for the entire reach under investigation. However, we highly advise performing independent column studies like those presented here in order to test the plausibility of the reactive parameters.

## Appendix A

### Derivation of the travel-time based model

The transport of fluorescein, Raz, and Rru is discussed above using the standard advection-dispersion equation for physical transport. Here we derive the equations in a travel-time framework. We closely follow the concept and the notation presented by Liao et al. (2013).

Because fluorescein is considered to behave conservatively (Smith and Pretorius, 2002; Kasnavia et al., 1999), the BTC  $c_{\text{out,Flu}}$  [ $\text{ML}^{-3}$ ] of fluorescein in the outflow is related to the travel-time distribution through the column  $g_0(\tau)$  [ $\text{T}^{-1}$ ] and the fluorescein concentration  $c_{\text{in,Flu}}$  [ $\text{ML}^{-3}$ ] by the following convolution integral:

$$c_{\text{out,Flu}}(t) = \int_0^{\infty} g_0(\tau) c_{\text{in,Flu}}(t - \tau) d\tau \quad (\text{A1})$$

in which  $t$  [T] is the time since the start of the injection and  $\tau$  [T] is the residence time in the column.  $g_0(\tau)$  is also the transfer-function of fluorescein and can be estimated by non-parametric deconvolution (Cirpka et al., 2007).

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The transport of Raz and Rru through the column is modified by equilibrium and kinetic sorption as well as decay processes. Rru was not injected into the column and thus solely originates from the transformation of Raz in the column itself. To calculate the concentrations of Raz and Rru at the outlet of the column, we can convolute the respective input signal of Raz  $c_{in,1}$  [ $ML^{-3}$ ] with the transfer functions  $g_1(\tau)$  [ $T^{-1}$ ], expressing the response of Raz in the outlet due to a unit pulse of Raz in the inlet, and  $g_{12}(\tau)$  [ $T^{-1}$ ], expressing the response of Rru in the outlet due to a unit pulse of Raz in the inlet, by:

$$c_{out,1}(t) = \int_0^{\infty} g_1(\tau) c_{in,1}(t - \tau) d\tau \quad (A2)$$

$$c_{out,2}(t) = \int_0^{\infty} g_{12}(\tau) c_{in,1}(t - \tau) d\tau \quad (A3)$$

As discussed in the following, we solve transport in the travel-time domain rather than the spatial domain. This has the advantage that the validity of the estimated sorption and transformation parameters does not depend on conservative transport to meet an analytical solution of the advection-dispersion equation. The outlet simply samples a conservative travel-time distribution, expressed by  $g_0(\tau)$ , which implies that the transfer functions  $g_1(\tau)$  and  $g_{12}(\tau)$  of Raz and Rru at the outlet are weighted averages of the transfer functions for all travel times  $\tau_*$  sampled by the outlet:

$$g_1(\tau) = \int_0^{\infty} g_0(\tau_*) c_1(\tau, \tau_*) d\tau_* \quad (A4)$$

$$g_{12}(\tau) = \int_0^{\infty} g_0(\tau_*) c_2(\tau, \tau_*) d\tau_* \quad (A5)$$

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in which  $c_i(\tau, \tau_*)$  [ $T^{-1}$ ] is the concentration response of Raz and Rru to a pulse of Raz at travel time  $\tau_*$  and time  $\tau$  since the pulse release. The governing equations for the transport of Raz and Rru through the column resulting from a point release in the inlet read as:

$$5 \quad \left(K_1^{\text{eq}} + 1\right) \frac{\partial c_1}{\partial \tau} + K_1^{\text{kin}} \frac{\partial c_{1,\text{kin}}}{\partial \tau} + \frac{\partial c_1}{\partial \tau_*} = -(\lambda_1 + \lambda_{12})c_1 \quad (\text{A6})$$

$$\left(K_2^{\text{eq}} + 1\right) \frac{\partial c_2}{\partial \tau} + K_2^{\text{kin}} \frac{\partial c_{2,\text{kin}}}{\partial \tau} + \frac{\partial c_2}{\partial \tau_*} = \lambda_{12}c_1 - \lambda_2c_2 \quad (\text{A7})$$

and

$$\frac{\partial c_{i,\text{kin}}}{\partial \tau} = k_i(c_i - c_{i,\text{kin}}) \quad (\text{A8})$$

10 subject to

$$c_i(\tau, \tau_* = 0) = \begin{cases} \delta(\tau) & \text{if } i = 1 \\ 0 & \text{otherwise} \end{cases}, c_i(\tau = 0, \tau_* > 0) = 0 \forall i \quad (\text{A9})$$

in which  $\delta(\cdot)$  is the Dirac delta function with inverse units of the argument. Note that in Eqs. (A4–A9)  $c_i$  and  $c_{i,\text{kin}}$  have units of inverse times, because they are not actual concentrations, which is in contrast to Eqs. (1–3), in which no convolution with input signals is performed.

15 Equations (A6–A9) can conveniently be solved in the Laplace domain:

$$\begin{aligned} \tilde{c}_1(s, \tau_*) &= \exp(-\beta_1 \tau_*) \\ \tilde{c}_2(s, \tau_*) &= d_2 \exp(-\beta_2 \tau_*) + d_{12} \exp(-\beta_1 \tau_*) \end{aligned} \quad (\text{A10})$$



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**Table 1.** Characteristics of the sediments used in the experiments.

	Steinlach	Goldersbach
Grain sizes	0.08–4 mm	0.08–4 mm
Grain density	2.60 kg L <sup>-1</sup>	2.58 kg L <sup>-1</sup>
Organic carbon content*	0.73 %	0.13 %
CaCO <sub>3</sub> content*	66.0 %	8.9 %
Specific surface area	9.92 m <sup>2</sup> g <sup>-1</sup>	18.45 m <sup>2</sup> g <sup>-1</sup>
Intragranular porosity	0.04	0.06

\* Contents are stated as percent by weight.

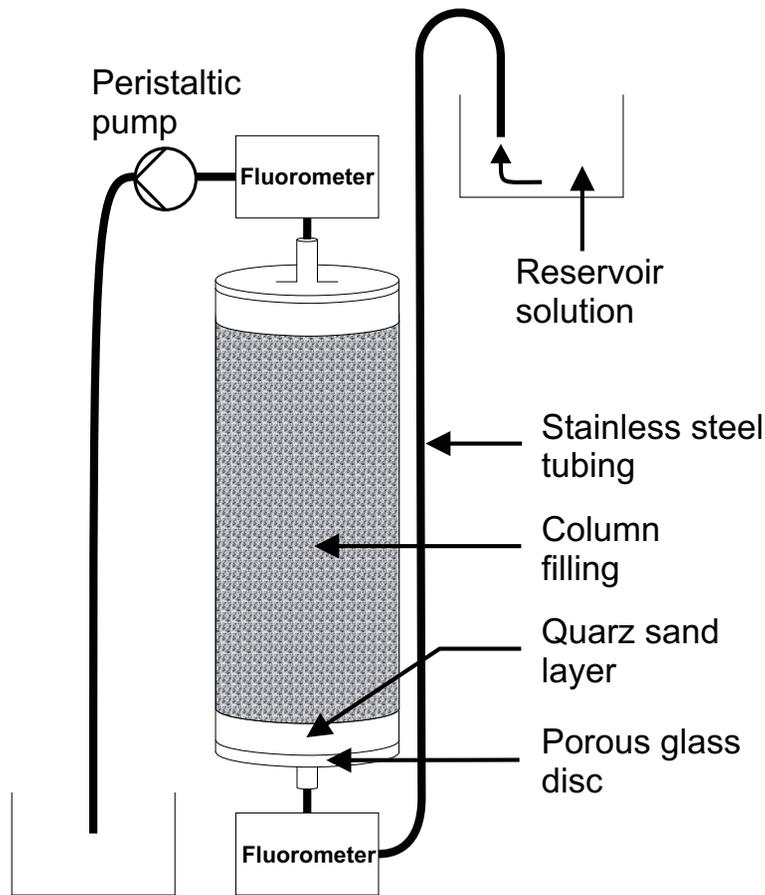
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**Table 2.** Maximum-likelihood parameter values describing sorption properties obtained by the column experiments. Bottom rows: comparison between values of distribution coefficients  $K_{d,i}^{\text{column}}$  and  $K_{d,i}^{\text{batch}}$  between all sorption sites and water in the column and batch experiments.

	Steinlach		Goldersbach	
	pH 7	pH 9	pH 7	pH 9
$K_{\text{Raz}}^{\text{eq}} [-]$	$0.18 \pm 0.007$	$0.04 \pm 0.001$	$0.01 \pm 0.003$	$0.00 \pm 0.001$
$K_{\text{Rru}}^{\text{eq}} [-]$	$0.00 \pm 0.001$	$0.01 \pm 0.000$	$0.25 \pm 0.008$	$0.06 \pm 0.006$
$K_{\text{Raz}}^{\text{kin}} [-]$	$0.82 \pm 0.013$	$0.79 \pm 0.001$	$0.49 \pm 0.015$	$0.09 \pm 0.006$
$K_{\text{Rru}}^{\text{kin}} [-]$	$0.29 \pm 0.007$	$0.66 \pm 0.004$	$1.35 \pm 0.088$	$1.64 \pm 0.118$
$k_{\text{Raz}} [\text{s}^{-1}] \times 10^{-4}$	$3.27 \pm 0.114$	$1.63 \pm 0.276$	$19.52 \pm 1.309$	$15.18 \pm 1.232$
$k_{\text{Rru}} [\text{s}^{-1}] \times 10^{-4}$	$50.67 \pm 2.365$	$4.77 \pm 0.319$	$1.97 \pm 0.150$	$2.71 \pm 0.185$
$\lambda_1 [\text{s}^{-1}] \times 10^{-5}$	$3.56 \pm 0.332$	$0.06 \pm 0.092$	$0.22 \pm 0.178$	$3.68 \pm 0.107$
$\lambda_{12} [\text{s}^{-1}] \times 10^{-5}$	$57.22 \pm 0.113$	$6.67 \pm 0.011$	$41.46 \pm 0.163$	$4.45 \pm 0.013$
$\lambda_2 [\text{s}^{-1}] \times 10^{-5}$	$0.04 \pm 0.088$	$0.49 \pm 0.551$	$0.27 \pm 0.196$	$1.30 \pm 0.597$
$K_{d_{\text{Raz}}}^{\text{column}} [\text{L kg}^{-1}]$	0.21	0.12	0.08	0.02
$K_{d_{\text{Rru}}}^{\text{column}} [\text{L kg}^{-1}]$	0.06	0.10	0.25	0.30
$K_{d_{\text{Raz}}}^{\text{batch}} [\text{L kg}^{-1}]$	1.90	0.63	2.97	1.00
$K_{d_{\text{Rru}}}^{\text{batch}} [\text{L kg}^{-1}]$	1.21	0.66	2.27	0.97

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**Fig. 1.** Schematic of the column experiments used to investigate the sorption of Raz and Rru.

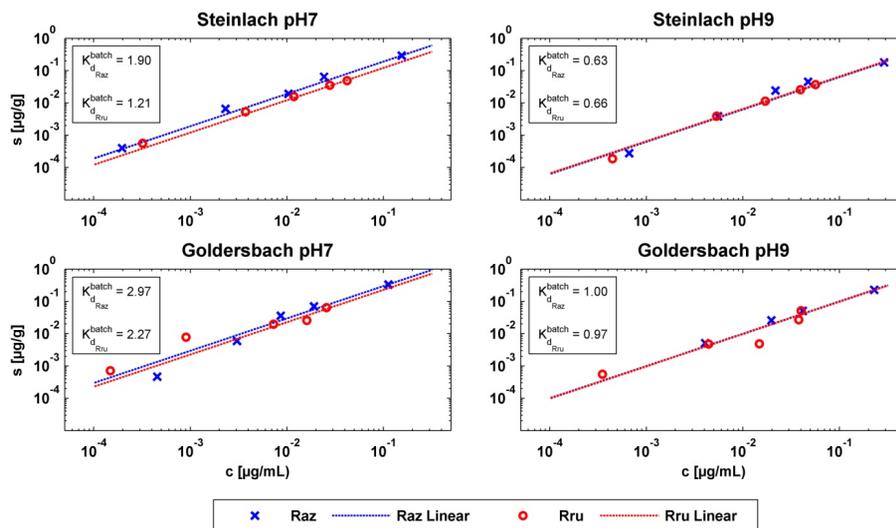
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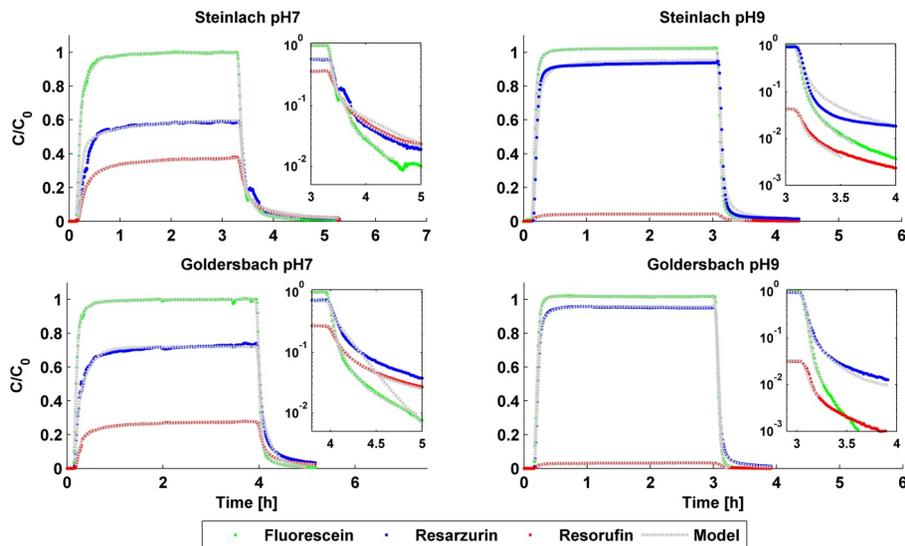


**Fig. 2.** Linear sorption isotherms of Raz and Rru for the different pH values and sediment types. All data are available in the Supplement. Values of  $K_{d_i}^{batch}$  in  $L\,kg^{-1}$ .

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## Sorption and transformation of the reactive tracers Raz and Rru

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**Fig. 3.** Measured and modeled tracer BTCs (column outlets) for fluorescein, Raz and Rru at pH 7 and pH 9 and for both sediments.

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